

### CLAIMS AMENDMENTS

1.-7. (Cancelled)

8. (Currently amended) Process for catalytic fluorination of saturated or olefinic halogenated hydrocarbon(s), the process comprising

providing a bulk catalyst has having a Ni/Cr atomic ratio between 0.02 and 0.4:1 prepared by

(a) impregnating an amorphous chromium III oxide with a solution of a nickel compound, wherein the chromium oxide has a BET specific surface area of greater than 150 m<sup>2</sup>/g and a pore volume of greater than 0.15 ml/g,

(b) drying the chromium oxide under an inert gas or under air at a temperature of between about 100° C and about 350° C, and

(c) activating the chromium oxide first with HF introduced diluted in air or in an inert gas at a temperature ranging from 150° C and 200° C and then with HF at a temperature less than 400 ° C; and

fluorinating the saturated or olefinic halogenated hydrocarbon(s) with HF in a gas phase in the presence of the bulk catalyst.

9. (Canceled).

10. (Canceled).

11. (Previously Presented) Process according to Claim 8, wherein the saturated or olefinic halogenated hydrocarbon(s) is fluorinated at a temperature between 50° C and 500°C.

12. (Previously Presented) Process according to Claim 8, wherein the saturated or olefinic halogenated hydrocarbon(s) is fluorinated for between 3 and 100 seconds.

13. (Previously Presented) Process according to Claim 8, wherein the molar ratio of HF/halogenated hydrocarbon(s) is between 1/1 and 30/1.

14. (Previously Presented) Process according to Claim 8, wherein the fluorination of the saturated or olefinic halogenated hydrocarbon(s) is carried out at an absolute pressure of between 0.08 and 2 MPa.

15. (Previously Presented) Process according to Claim 8, wherein the fluorination of the saturated or olefinic halogenated hydrocarbon(s) is carried out in the presence of an oxidizing agent.

16. (Previously Presented) Process according to Claim 8, further comprising deactivating the bulk catalyst by coking; and regenerating the catalyst with a treatment with air or with oxygen or by a  $\text{Cl}_2/\text{HF}$  mixture, at a temperature of between 250° C and 400°C.

17. (Previously Presented) Process according to Claim 8, wherein the halogenated hydrocarbon(s) is perchloroethylene or 1-chloro-2,2,2-trifluoroethane.

18. (Previously Presented) Process according to Claim 8, wherein the catalyst is activated with pure HF at the temperature between 350° C and 380°C.

19. (Previously Presented) Process according to Claim 11, wherein the fluorination temperature is between 100° C and 450°C.

20. (Previously Presented) Process according to Claim 11, wherein the fluorination temperature is between 120° C and 400°C.

21. (Previously Presented) Process according to Claim 12, wherein the fluorination time is less than 30 seconds.

22. (Previously Presented) Process according to Claim 13, wherein the molar ratio of the HF in the gas phase to the halogenated hydrocarbon(s) is less than 20/1.

23. (Previously Presented) Process according to Claim 14, wherein the pressure is between 0.1 and 1.5MPa.

24. (Previously Presented) Process according to Claim 15, wherein the oxidizing agent is air or oxygen.

25. (New) Process for catalytic fluorination of saturated or olefinic halogenated hydrocarbon(s), the process comprising  
providing a bulk catalyst having a Ni/Cr atomic ratio between 0.02 and 0.4:1 prepared by

(a) impregnating an amorphous chromium III oxide with a solution of a nickel compound, wherein the chromium oxide has a BET specific surface area of greater than 150  $\text{m}^2/\text{g}$  and a pore volume of greater than 0.15 ml/g,

(b) drying the chromium oxide under an inert gas or under air at a temperature of between about 100° C and about 350° C, and

(c) activating the chromium oxide first with HF introduced diluted in air or in an inert gas at a temperature ranging from 150° C and 200° C and then with HF at a temperature less than 400 ° C; and

fluorinating the saturated or olefinic halogenated hydrocarbon(s) with HF in a gas phase in the presence of the bulk catalyst; and the saturated or olefinic halogenated hydrocarbon(s) is fluorinated for between 3 and 100 seconds.